Ya. M. Naziev, M. M. Bashirov, and Yu. A. Badalov

Results of measurements of isobaric specific heat of n-octyl and n-nonyl alcohols and n-hexane are presented.

Study of the dependence of thermophysical properties of aliphatic alcohols on temperature and pressure is important in connection with the ever wider use of these substances in technological processes.

The goal of the present study, which is a continuation of [1], is an experimental investigation of isobaric specific heat ( $c p$ ) of two representatives of the normal alcohols, $n$ octyl and n-nonyl, at high pressures and various temperatures.

The experiments were performed with impulsive regular regime equipment to determine the isobaric volume specific heat of the liquids. A description of the equipment and measurement methods are presented in [1, 2].

Values of $c^{\prime} p$ of $n$-octyl and n-nonyl alcohols were measured at temperatures of 303.1$523.15^{\circ} \mathrm{K}$ and pressures of $0.1-50 \mathrm{MPa}$. In addition $c^{\prime} \mathrm{p}$ of n -hexane was measured at the same state parameters, as a control, in order to confirm the reliability of the data obtained for the alcohols, since the specific heat of $n$-hexane at high pressures has been studied quite thoroughly [3-7].

The n-octyl and n-nonyl alcohols and the n-hexane used in the experiments were of the "Ch" purity grade, with purities of $99.6,99.4$, and $99.8 \%$, respectively, with the following characteristics:

$$
\begin{array}{lll}
\rho_{4}^{20}=825,8 \mathrm{~kg} / \mathrm{m}^{3} ; & n_{D}=1,4288 ; & T_{\mathrm{b}}=468,43 \mathrm{~K} ;
\end{array} T_{\mathrm{f}}=258,15 \mathrm{~K} ; ~\left(\begin{array}{ll}
20 \\
\rho_{4}^{20}=827,8 \mathrm{~kg} / \mathrm{m}^{3} ; & n_{D}=1,4336 ;
\end{array} T_{\mathrm{b}}=486,65 \mathrm{~K} ; \quad T_{\mathrm{f}}=268,15 \mathrm{~K} ;\right.
$$

The experimental data on isobaric specific heat of the alcohols at high pressure were obtained for the first time.

The experiments were carried out along isotherms, with temperature steps of $\sim 25^{\circ} \mathrm{K}$. On all the isotherms $c^{\prime} p$ was measured at pressure values of $0.1,2.5,5.0,10.0,20.0,30.0$, 40.0 , 50.0 MPa .

Isobaric (volume) specific heat $c$ 'p values were calculated with the following computation equation derived in [2]:

$$
\begin{equation*}
c_{p}^{\prime}=\frac{1}{V\left(1+\frac{2 \delta}{3 R_{1}}+\frac{2 \delta^{\prime}}{3 i}\right)}\left[\frac{W(1-K)}{b}-M_{\mathrm{b}} c_{\mathrm{b}}\right] \tag{1}
\end{equation*}
$$

where $K=W_{\text {loss }} / W$.
The experiments revealed that the value of $K$ was not dependent on pressure, and that it was desirable to determine the temperature dependence $K=f(T)$ by control measurements on one isobar for well-studied substances. Water and benzol can be recommended for this purpose, since experimental data on $c_{p}$ and $c^{\prime} p$ for these liquids are most reliable.

[^0]TABLE 1. Isobaric Mass $c_{p} \cdot 10^{-3}, \mathrm{~J} /(\mathrm{kg} \cdot \mathrm{K})$ and Volume $\mathrm{c}^{\prime} \mathrm{p} \cdot$ $10^{-3}, \mathrm{~J} /\left(\mathrm{m}^{3} \cdot \mathrm{~K}\right)$ Specific Heats of n -Hexane


TABLE 2. Isobaric Mass $c_{p} \cdot 10^{-3}, J /(k g \cdot K)$ and Volume $c^{\prime} p^{\prime}$ $10^{-3}, \mathrm{~J} /\left(\mathrm{m}^{3} \cdot \mathrm{~K}\right)$ Specific Heats of n -Octyl Alcohol

| $T, \mathrm{~K}$ | P. MPa |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0,1 |  | 2,5 |  | 5,0 |  | 10 |  |
|  | ${ }^{c} p$ | $c^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ |
| 303,2 | 2,53 | 2064,2 | 2,527 | 2065,0 | 2,524 | 2066,1 | 2,52 | 2069,9 |
| 323,65 | 2,637 | 2113,6 | 2,633 | 2114,8 | 2,629 | 2116,4 | 2,625 | 2120,8 |
| 350,45 | 2,779 | 2173,2 | 2,775 | 2175,6 | 2,77 | 2177,2 | 2,763 | 2181,4 |
| 371,55 | 2,896 | 2216,0 | 2,889 | 2218,2 | 2,882 | 2220,3 | 2,873 | 2224,6 |
| 400,15 | 3,052 | 2263,0 | 3,043 | 2265,1 | 3,032 | 2268,2 | 3,019 | 2274,6 |
| 422,65 | 3,182 | 2297,4 | 3,168 | 2298,4 | 3,153 | 2300,4 | 3,135 | 2307,3 |
| 448,65 | 3,347 | 2326,0 | 3,315 | 2325,2 | 3,296 | 2329,0 | 3,273 | 2336,5 |
| 476,60 | - | - | 3,476 | 2352,0 | 3,456 | 2353,5 | 3,42 | 2363,2 |
| 499,65 | - | - | 3,626 | 2364, 3 | 3,595 | 2368,1 | 3,55 | 2377,3 |
| 523,15 | - | - | 3,792 | 2374,0 | 3,76 | 2380, 1 | 3,704 | 2393,3 |
| $\tau, \mathrm{K}$ | $P$. MPa |  |  |  |  |  |  |  |
|  | 20 |  | 30 |  | 40 |  | 50 |  |
|  | ${ }^{c} p$ | $c_{p}^{\prime}$ | $c_{p}$ | $c^{\prime \prime}$ | $c_{p}$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c{ }_{p}^{\prime \prime}$ |
| 303,2 | 2,516 | 2080,2 | 2,512 | 2089,0 | 2,508 | 2097,2 | 2,505 | 2105,5 |
| 323,65 | 2,62 | 2132,7 | 2,615 | 2143,0 | 2,61 | 2153,3 | 2,606 | 2163,0 |
| 350,45 | 2,755 | 2195,0 | 2,748 | 2209,4 | 2,741 | 2220, 2 | 2,735 | 2231,8 |
| 371,55 | 2,863 | 2239,4 | 2,854 | 2255,2 | 2,846 | 2268,3 | 2,839 | 2281, 1 |
| 400,15 | 3,006 | 2291,7 | 2,994 | 2309,0 | 2,983 | 2325,6 | 2,974 | 2341,1 |
| 422,65 | 3,115 | 2326,0 | 3,10 | 2345,1 | 3,088 | 2364,3 | 3,078 | 2381,5 |
| 448,65 | 3,245 | 2357,0 | 3,225 | 2380,1 | 3,212 | 2401, 8 | 3,20 | 2421,9 |
| 476,60 | 3,385 | 2388,1 | 3,360 | 2413,8 | 3,34 | 2435,6 | 3,325 | 2461,8 |
| 499,65 | 3,51 | 2407,8 | 3,477 | 2436,7 | 3,455 | 2461,9 | 3,435 | 2490,0 |
| 523,15 | 3,638 | 2423,0 | 3,595 | 2452,0 | 3,57 | 2482,8 | 3,55 | 2515, |

On the basis of the experimental data obtained for $c^{\prime} p$ the isobaric (mass) specific heat $c_{p}$ was calculated, for which step a knowledge of the density of the materials studied is required. Density values for $n$-ocyl and $n$-nonyl alcohols and $n$-hexane were taken from [8-10]. Results of the $c_{p}$ and $c^{\prime} p$ measurements are presented in Tables 1-3.


Fig. 1. Comparison of isobaric specific heat data for n-octyl (a) and n-nonyl (b) alcohols at atmospheric pressure: a: 1) present data; 2) [13]; 3) [11]; b: 1) present data; 2: [13]; 3) [12].

TABLE 3. Isobaric Mass $c_{p} \cdot 10^{-3}, \mathrm{~J} /(\mathrm{kg} \cdot \mathrm{K})$ and Volume $\mathrm{c}_{\mathrm{p}} \cdot 10^{-3}$, $J /\left(\mathrm{m}^{3} \cdot \mathrm{~K}\right)$ Specific Heats of n -Octyl Alcohol

| $T, \mathrm{~K}$ | $P, \mathrm{MPa}$ |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.1 |  | 2,5 |  | 5 |  | 10 |  |
|  | ${ }^{c} p$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ | ${ }^{c} p$ | $c_{p}^{\prime}$ |
| 303,1 | 2,470 | 2029,8 | 2,467 | 2031,1 | 2,463 | 2032,0 | 2,46 | 2035,9 |
| 325,95 | 2,594 | 2094,3 | 2,59 | 2095,3 | 2,585 | 2096,5 | 2,58 | 2099,6 |
| 351,35 | 2,730 | 2155,7 | 2,723 | 2156,6 | 2,716 | 2157,6 | 2,709 | 2160,4 |
| 374, 15 | 2,854 | 2205,0 | 2,848 | 2208,4 | 2,84 | 2211,0 | 2,833 | 2215,4 |
| 401,55 | 2,995 | 2252,0 | 2,986 | 2254,4 | 2,979 | 2258,0 | 2,968 | 2261,3 |
| 427,65 | 3,132 | 2287,01 | 3,117 | 2288,9 | 3,108 | 2292,1 | 3,094 | 2297,3 |
| 450,05 | 3,263 | 2312,0 | 3,245 | 2313,9 | 3,228 | 2316,0 | 3,205 | 2321,2 |
| 474,15 | 3,42 | 2340,9 | 3,385 | 2337, 3 | 3,362 | 2339,1 | 3,33 | 2344,4 |
| 498,45 | - | - | 3,541 | 2354,6 | 3,51 | 2359,0 | 3,467 | 2365,9 |
| 522,45 | - | - | 3,713 | 2367,0 | 3,663 | 2373,1 | 3,605 | 2381,1 |
| T, K | $P, \mathrm{MPa}$ |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |
|  | 20 |  | 30 |  | 40 |  | 50 |  |
|  | ${ }^{c} p$ | ${ }^{c} p$ | ${ }^{c} p$ | ${ }^{c} p$ | ${ }^{c} p$ | ${ }^{c} p$ | ${ }^{c} p$ | $c_{p}$ |
| 303,1 | 2,456 | 2045,8 | 2,452 | 2054 | 2,448 | 2062,7 | 2,445 | 2072, 1 |
| 325,95 | 2,574 | 2110,2 | 2,568 | 2119,0 | 2,564 | 2128,1 | 2,56 | 2137,6 |
| 351,35 | 2,703 | 2173,2 | 2,698 | 2185,4 | 2,693 | 2195,1 | 2,688 | 2205,5 |
| 374,15 | 2,825 | 2227,1 | 2,817 | 2242,3 | 2,811 | 2254,4 | 2,805 | 2265,5 |
| 401,55 | 2,955 | 2278,0 | 2,947 | 2295,1 | 2,941 | 2310,2 | 2,935 | 2327,4 |
| 427,65 | 3,077 | 2315,0 | 3,068 | 2337, 8 | 3,062 | 2356,2 | 3,058 | 2375,0 |
| 450,05 | 3,182 | 2341,4 | 3,171 | 2365,6 | 3,162 | 2387,0 | 3,158 | 2410,0 |
| 474,15 | 3,3 | 2369,0 | 3,281 | 2393,5 | 3,272 | 2419,8 | 3,267 | 2445,1 |
| 498,45 | 3,423 | 2392,0 | 3,399 | 2420,0 | 3,385 | 2449,0 | 3,379 | 2477,1 |
| 522,45 | 3,545 | 2411,8 | 3,516 | 2443,5 | 3,50 | 2475,0 | 3,492 | 2505,0 |

The data obtained for $c_{p}$ of $n$-hexane were compared to the results of [3-7]. In [3-5] the isobaric specific heat of $n$-hexane was studied by the flow adiabatic calorimeter method with a closed circulation system at pressures of $0.1-60 \mathrm{MPa}$ and temperatures from 293.15 to $624.3^{\circ} \mathrm{K}$. Comparison of experimental data on $c_{p}$ of $n$-hexane with available values at atmospheric pressure [3, 4] revealed that the data of [3, 4] are low in value by a maximum of $1.7 \%$. Comparison at high temperatures and pressures showed that the results of [4, 5] are low by an average of $3.0 \%$, and in individual cases - at 40.0 MPa pressure and $447.15^{\circ} \mathrm{K}$ temperature - the divergence reaches $5.2 \%$.

In [6] the isobaric specific heat of $n$-hexane was measured by the Tian-Calvet method (relative variant) at the single temperature of $298.15^{\circ} \mathrm{K}$ and pressures from 0.098 to 147 MPa. Considering that our measurements of n-hexane $c_{p}$ commenced from $308.35^{\circ} \mathrm{K}$, for comparison purposes the data was extrapolated to a temperature of $298.15^{\circ} \mathrm{K}$. The divergence of the data of [6] comprised $2.0 \%$ at atmospheric pressure, increasing to $6.0 \%$ at high ( 50.0 MPa ) pressure.


Fig. 2. Volume isobaric specific heat of n-octyl alcohol vs temperature and pressure: 1) $\mathrm{T}=303.2{ }^{\circ} \mathrm{K}$; 2) 323.65 ; 3) 350.45; 4) 371.55 ; 5) 400.15; 6) 422.65 ; 7) 448.65 ; 8) 476.60 ; 9) $523.15^{\circ} \mathrm{K}$; I) $\mathrm{P}=0.1 \mathrm{MPa}$; II) 10.0; III) 20; IV) 30 ; V) 40; VI) 50 .

Hadden [7] proposed a generalized equation for calculation of isobaric specific heat of liquid n-alkanes from the fusion temperture to the boiling point at atmospheric pressure. The calculated values of $n$-hexane $c_{p}$ computed with Hadden's expression were compared to the present experimental data, and a maximum divergence of no more than $2.6 \%$ was found.

Thus, the divergence of data available in the literature from the present data at low pressures lies in the range $2.0-2.5 \%$, which is essentially within the limits of experimental uncertainty for determination of $c_{p}$ of liquids.

There have been only a limited number of studies of isobaric specific heat of $n$-ocyl and n-nonyl alcohols, providing data only at atmospheric pressure [11-13]. Temperature intervals for study of $c_{p}$ comprise: in [11] for n-ocyl $313.15-468.15^{\circ} \mathrm{K}$, in [12] for n-nonyl $303.15-483.15^{\circ} \mathrm{K}$, and in [13] for n-octyl $310.67-452.29^{\circ} \mathrm{K}$ and for $n-n o n y 1 \quad 304.17-464.24^{\circ} \mathrm{K}$. Results of a comparison of the present experimental data at atmospheric pressure with data of [11-13] for $c_{p}$ of $n$-octyl and n-nonyl alcohols are shown in Fig. 1 , whence it is evident that the maximum deviations of the data of [11, 13] for n-octyl alcohol are 6.4 and $4.3 \%$, respectively, while for n-nonyl alcohol the divergences from the data of [12, 13] do not exceed 5.3 and $4.7 \%$, respectively.

Since data on isobaric specific heat of n-octyl and n-nonyl alcohols at high pressures have been obtained for the first time in the present study, it is impossible to compare them to other values.

To better clarify the dependence $c^{\prime} p=f(P, T)$ for n-octyl alcohol we present the data graphically in Fig. 2. It is evident that with increase in temperature and growth in pressure $c^{\prime} p$ increases. A similar pattern was also found for n-nonyl alcohol.

To generalize the $c_{p}$ data obtained the $c_{p}-\rho$ relationship proposed in [14] for liquid toluol ( $5.0,10.0,20.0,30.0 \mathrm{MPa}$ isobars) was used. For the spirits studied a slight layering over isobars was observed, especially noticable at pressures above 30.0 MPa .

The dependence can be expressed in the form of interpolation equations

$$
\begin{equation*}
c_{p}=10^{3} \sum_{i=1}^{n} A_{i}\left(\frac{\rho}{100}\right)^{i-1} \tag{2}
\end{equation*}
$$

To approximate Eq. (2) in polynomial form and determine the optimum value of $n$ by the method of least squares a FORTRAN program for the ES-1022 computer was developed. The program permitted determination of the polynomial coefficients to the sixth degree with subsequent calculation of mean square deviations from smoothed curves. As a result the optimal degree of the polynomial was determined, corresponding to minimum mean square deviation. In the present case for Eq. (2) $n=2$, i.e., a rectilinear dependence was obtained for all isobars of the alcohols studied. Values of the coefficients of Eq. (2) are presented in Table 4.

To consider the effect of layering over isobars in the coefficients $A_{1}$ and $A_{2}$ in Eq. (2) we introduce a parameter $P$ :

TABLE 4. Coefficients of Eq. (2)

| Substance | Coefficient | P, MPa |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 0.1 | 2.5 | 5 | 10 |
| n-Octyl alcohol | $A_{1}$ $A_{2}$ | 8,048005 $-0,674715$ | 7,899964 $-0,654662$ | $\begin{array}{r} 7,935562 \\ -0,658120 \end{array}$ | $\begin{array}{r} 8,031140 \\ -0,668019 \end{array}$ |
| n-Nonyl alcohol | $A_{1}$ $A_{2}$ | $\begin{array}{r} 8,107812 \\ -0,682409 \end{array}$ | 7,939711 $-0,659655$ | $\begin{array}{r} 8,011864 \\ -0,667634 \end{array}$ | $\begin{array}{r} 8,079167 \\ -0,674199 \end{array}$ |
| Substance | Coefficient | $P, \mathrm{M} \mathrm{Pa}$ |  |  |  |
|  |  | 20 | 30 | 40 | 50 |
| n-Octyl alcohol | $A_{1}$ $A_{2}$ | 8,256345 $-0,691199$ | 8,518218 $-0,718792$ | 8,774221 $-0,745770$ | $\begin{array}{r} 9,126382 \\ -0,784318 \end{array}$ |
| n-Nonyl alcohol | $A_{1}$ $A_{2}$ | 8,299903 $-0,696774$ | 8,648950 $-0,735472$ | 8,966676 $-0,770027$ | $\begin{array}{r} 9,246096 \\ -0,799280 \end{array}$ |

TABLE 5. Coefficients of Eqs. (3), (4)

| Substance | Coefficient |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $B_{1}$ | $B_{2}$ | $B_{3}$ | $C_{1}$ | $C_{2}$ | $C_{3}$ |  |
| n-Octyl <br> alcohol <br> n-Nony1 <br> alcohol | 7,9382437 | 0,0091516 | 0,0002968 | $-0,6608405$ | $-0,0006917$ | 0,00003613 |  |

$$
\begin{align*}
& A_{1}=\sum_{j=1}^{m} B_{j} \cdot P^{j-1}  \tag{3}\\
& A_{2}=\sum_{\varepsilon=1}^{k} C_{\varepsilon} \cdot P^{\varepsilon-1} \tag{4}
\end{align*}
$$

The method described above was used to determine the optimal degree of polynomials (3) and (4) $: m=k=3$ and the values of the coefficients $B_{j}, C_{\varepsilon}$, which are presented in Table 5.

Equations (2)-(4) can be used for interpolation and extrapolation of $c_{p}$ data for the alcohols studied.

## NOTATION

$c^{\prime} p$, volume specific heat, $J /\left(\mathrm{m}^{3} \cdot \mathrm{~K}\right)$; $c_{p}$, isobaric specific heat, $J /(\mathrm{kg} \cdot \mathrm{K})$; $\rho$, density of material in ampul, $\mathrm{kg} / \mathrm{m}^{3} ; \mathrm{b}=\Delta t / \Delta \tau$, heating rate at given temperature, $\mathrm{K} / \mathrm{sec}$; W , internalheater power, $W$; Wloss, correction for the thermal power losses, $W$; Mbcb, total ballast heat capacity of ampul, $J / \mathrm{K} ; \delta, \delta^{\prime}$, thicknesses of annular and plane end liquid layers, $m ; R_{1}, l$, ampul radius and length, $m$; $T$, thermodynamic temperature, ${ }^{\circ} \mathrm{K} ; \mathrm{P}$, pressure, MPa ; $\mathrm{T}, \mathrm{T}$, fusion and boiling points of substance, ${ }^{\circ} \mathrm{K} ; \mathrm{nD}$, index of refraction; $A_{i}, B_{j}, C_{\varepsilon}$, equation constants; $\mathrm{n}, \mathrm{m}, \mathrm{k}$, degrees of polynomials.

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VISCOELASTIC PROPERTIES OF THERMOTROPIC LIQUID CRYSTAL
POLYMERS FROM ANALYSIS OF DYNAMICAL CHARACTERISTICS
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UDC 532.135

The rheological properties of liquid-crystal polymers with side-chain mesogenic groups are studied by means of small-amplitude periodic deformations in the mesophase and in the isotropic melt.

Thermotropic liquid-crystal polymers have been studied intensively in recent years in connection with their structure and behavior [1]. Therefore it is important to be able to describe their behavior in the different physical states, in particular, the viscous fluid state. The rheological approach to the study of the physical-chemical and physical-mechanical properties of liquid-crystal polymers is very fruitful and highly informative, since the viscoelastic parameters depend strongly on the structure and phase-aggregate state of the system.

Examination of the literature shows that in the majority of papers devoted to discussions of the rheological properties of liquid-crystal systems, only the viscous characteristics of the systems are considered. This is true both for thermotropic linear polymer systems [1, 2] as well as for polymers with a comblike structure [3]. However it is well known that the most complete rheological behavior of a system reflects its viscoelastic characteristics, which have not been studied extensively for liquid-crystal polymers, and have been limited to only a few systems [4-7].

The rheological behavior of liquid-crystal polymers with lateral mesogenic groups connected directly to the principal chains is of significant interest, for the following reasons. First, in polymers systems of this type the principal chain actively participates in the formation of the liquid-crystal phase, and hence the mesophases of these systems are true polymers. In addition, the macromolecules of these polymers are characterized by low equilibrium and high kinetic rigidity of the principal chain [8]. Finally polymers of this type have a layered structure which develops reversibly with increasing temperature [9, 10]. The features of the layered ordering depend on the structure of the monomeric unit and affect the thermodynamic, relaxational, and other properties of the polymers. In particular, for the
 differential scanning calorimetry and linear thermodilatometry show that the parameters of the

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